

VARIATION IN ENTHALPY OF THE SYSTEM *n*-TETRACOSANE–*n*-HEXACOSANE AS FUNCTIONS OF TEMPERATURE AND COMPOSITION

Z. Achour-Boudjema, M. Bouroukba, D. Balesdent, E. Provost
and M. Dirand

Laboratoire de Thermodynamique Chimique et Appliquée, Ecole Nationale Supérieure des
Industries Chimiques, Institut National Polytechnique de Lorraine 1, rue Grandville, B.P. 451
F-54001 Nancy Cedex, France

(Received January 26, 1996; in revised form September 10, 1996)

Abstract

Differential enthalpy analyses were performed on the binary *n*-alkane system *n*-C₂₄H₅₀–*n*-C₂₆H₅₄ with a Setaram DSC111 calorimeter of Tian Calvet type.

The measurements provided enthalpy data from 260 to 260 K on *n*-tetracosane, *n*-hexacosane and 19 binary mixtures.

An analytical expression, derived from the Einstein model, is proposed for every pure phase in its temperature domain, to represent the variation in the enthalpy with temperature.

A general expression for the enthalpy as a function of temperature and composition is also given.

Keywords: binary mixtures, calorimetry, Einstein's solid model, enthalpy variations, *n*-hexacosane, *n*-tetracosane

Introduction

The phase diagram of the binary *n*-alkane system *n*-tetracosane (*n*-C₂₄H₅₀)–*n*-hexacosane (*n*-C₂₆H₅₄) was determined by means of joint calorimetric and radiocrystallographic studies.

At room temperature, this system shows the existence of two limited terminal solid solutions and three orthorhombic intermediate phases. The terminal solid solutions, denoted γ_1 and γ_2 , are isostructural with *n*-tetracosane and *n*-hexacosane [1, 2]. The intermediate phases, denoted β'_1 , β'' and β'_2 , are identical to those found in the system *n*-eicosane (*n*-C₂₀H₄₂)–*n*-docosane (*n*-C₂₂H₄₆) [3], and *n*-docosane (*n*-C₂₂H₄₆)–*n*-tetracosane (*n*-C₂₄H₅₀) [2, 4, 5]. They are isomorphic with the structure of *n*-tricosane (*n*-C₂₃H₄₈) and *n*-pentacosane (*n*-C₂₅H₅₂) [2, 6–12].

With increasing temperature, γ_1 and γ_2 behave in the same way as *n*-tetracosane and *n*-hexacosane [2, 13–15]. The solutions β'_1 , β'' and β'_2 undergo the same solid-state transitions as those observed in *n*-tricosane [2, 6–12] and in the binary system *n*-docosane–*n*-tetracosane [12, 15].

In this work, we present a differential calorimetric analysis of the system *n*-C₂₄H₅₀–*n*-C₂₆H₅₄. The enthalpy variation vs. temperature is given for the different solid phases. The data concerning the phases γ_1 , β'_1 , β'' and β'_2 are then treated by using functions derived from the Einstein solid model.

Finally, a general expression is given for the enthalpy of the solid solutions as a function of temperature and composition.

Experimental

The enthalpy measurements were performed with a DSC111 differential scanning calorimeter manufactured by Setaram.

The low-temperature measurements were carried out by adding a cooling device to the calorimeter, allowing the circulation of cold nitrogen in the calorimeter.

The apparatus was calibrated with the help of the thermodynamic data on alumina reported in the N.B.S. table [16].

Principle of measurement

The difference in heat flow exchanged between the two cells and the calorimeter block is evaluated by measurement of the electromotive force (*e.m.f.*) developed in two thermopiles surrounding the calorimeter cells and connected together in opposition.

The *e.m.f.* ΔE , measured from time t_1 to time t_2 , is related to the difference in heat Q_T exchanged between the cells and the calorimeter block, by means of the sensitivity coefficient S , determined by calibration:

$$Q_T = \frac{1}{S} \int_{t_1}^{t_2} \Delta E dt$$

– Q_T is computed by numerical integration, for each temperature jump $\Delta T = T_2 - T_1$ (T_1 and T_2 correspond, respectively, to time t_1 and time t_2). Q_T is split into two terms, Q_D and Q_E .

– Q_D corresponds to the disymmetry of the two cells. It is determined in a 'blank' measurement, by introducing an empty crucible into each of the two cells.

– Q_E corresponds to the sample contribution and $Q_E = Q_T - Q_D$.

– Q_T is obtained by putting the sample in one of the previous crucibles, the second remaining empty as reference.

The molar enthalpy of heating of the sample at temperature T , referred to 260 K, is

$$H(T) - H(260) = \sum_i \frac{M}{m} (Q_E)_i$$

where M and m are, respectively, the molar weight and the mass of the sample introduced in the calorimeter.

$H(T)$ and $H(260)$ are the enthalpies at T and 260 K, respectively.

Operating conditions

The measurements were carried out by sequential programming of the temperature vs. time:

- The rising temperature period t_m was set at 180 s and corresponded to 1 or 0.5 K, depending on the temperature range.
- The temperature level duration t_p depends on a computer test, checking that the calorimeter signal returned to constant value, corresponding to a steady state. When no transition occurred in the sample, $t_p=420$ s (Fig. 1).

As the signal might stabilize at a value that was not exactly the base line, an automatic correction was made by the computer (Fig. 2).

The measurements were performed in two steps, for both blank and sample:

- from 260 to 300 K, at a temperature rate of 20 K h^{-1} , giving a temperature jump of 1 K, using the cooling device;
- from 290 to 360 K, at a temperature rate of 10 K h^{-1} , giving a temperature jump of 0.5 K.

These two series of measurement overlap in a range of 10 K; no significant differences between the operating conditions were observed.

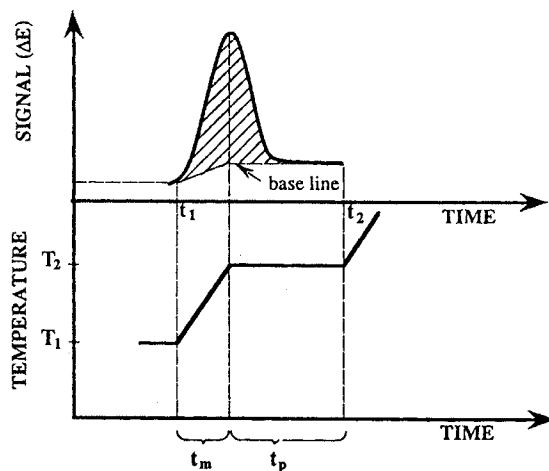


Fig. 1 Integration of the calorimetric signal

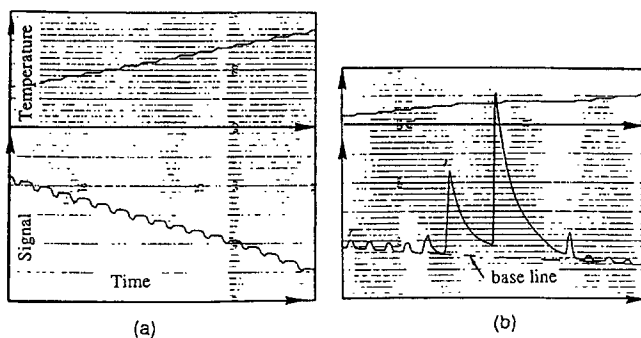


Fig. 2 Signal and temperature profiles for a discontinuous experiment. a – blank; b – sample

Sample preparation

The *n*-tetracosane and *n*-octacosane were purchased from Aldrich: their purity grade was 99%, as determined by gas chromatography and mass spectroscopy.

The samples (pure *n*-alkanes and mixtures) were prepared by weighing the solid components, melting and thorough mixing. The homogeneous liquids thus obtained were quenched in a crystallizing dish, maintained at a very low temperature in a Dewar vessel with liquid air. Such a rapid cooling ensured an uniform steric concentration in the solid.

Experimental results

Variation in enthalpy with temperature

The reproducibility and the precision of the enthalpy measurements were determined by using *n*-hexacosane, for which the experimental enthalpy was com-

Table 1 Enthalpy variation of standard alumina from "National Bureau of Standard [16] vs. temperature

T/K	$H_{\text{exp}}/\text{J mol}^{-1}$	$H_{\text{lit}}/\text{J mol}^{-1}$	Deviation/ J mol^{-1}	Relative deviation/%
289.4	0	0	0	0
300	874	826	48	5.4
310	1605	1631	-27	-1.7
320	2425	2456	-31	-1.3
330	3261	3301	-40	-1.2
340	4122	4163	-42	-1
350	4998	5043	-45	-1

T : temperature in Kelvins, H_{exp} : variation of the experimental enthalpy in J mol^{-1} , H_{lit} : variation of the enthalpy from literature in J mol^{-1} .

pared with literature data [16, 17]. The relative deviation was about 2% (Table 1 and 2).

The calorimetric measurements were made on *n*-tetracosane, *n*-hexacosane and 19 binary mixtures, covering the whole range of concentration. The results are presented in Tables 3–13. The enthalpy variations are given every 5 K, except for the solid transition and melting domains. Figure 3 presents the curve of the enthalpy for the mixture containing 32.5 mol% *n*-hexacosane.

Table 2 Enthalpy variation of *n*-hexacosane vs. temperature

<i>T</i> /K	$H_{exp}/J\ mol^{-1}$	$H_{lit}/J\ mol^{-1}$	Deviation/ $J\ mol^{-1}$	Relative deviation/%
270	0	0	0	–
280	6061	5920	141	2.3
290	12381	12110	270	2.2
300	18961	18580	381	2
310	25669	25480	189	0.7
320	32720	32780	–60	0.2
330	134897	134780	117	0.1
340	142731	143280	–549	0.4

T: temperature in Kelvins, H_{exp} : variation of the experimental enthalpy in $J\ mol^{-1}$, H_{lit} : variation of the enthalpy from literature [17] in $J\ mol^{-1}$.

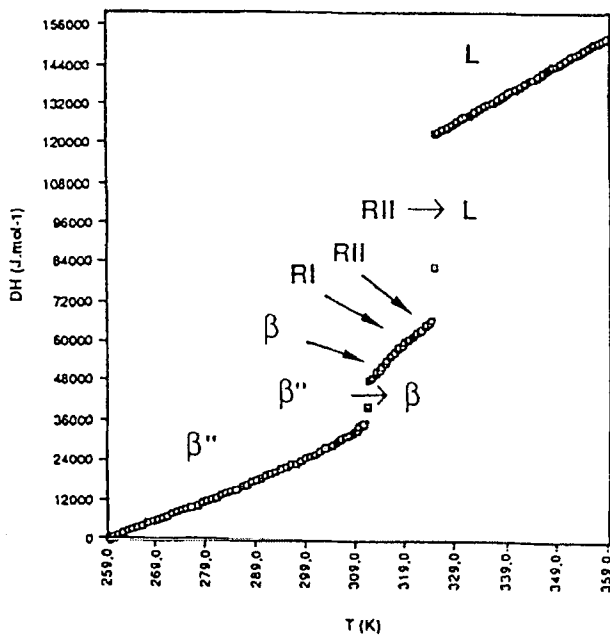


Fig. 3 Enthalpy curve for the mixture containing 32.5 mol% of *n*-hexacosane

Representation of the variations in enthalpy for the phases γ_1 , β_1' , β_2'' , β_2' and γ_2

We proposed to represent the binary system with the help of the Einstein model. Such a binary behaves like a monoatomic solid of N atoms, having $3N$ independent vibrations, which are harmonic and have the same frequency. This frequency corresponds to a typical temperature θ , called Einstein's temperature.

For each composition, the enthalpy variations can be described by the following expression, derived from the Einstein model:

Table 3 Variations of the enthalpy vs. temperature

T/K	C_{24} $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:1.1 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0	↑ γ_1 ↓	259.5	0	↑ γ_1 ↓
260.5	400		260.5	454	
265.5	2945		265.5	2545	
270.5	5134		270.5	5271	
275.5	7456		275.5	7860	
280.5	9856		280.5	9875	
285.4	12359		285.4	13477	
290.4	14866		290.4	16201	
295.4	17631		295.4	18689	
300.4	20434		300.4	21513	
305.4	25562		305.4	24575	
310.4	26068		310.4	27984	
315.4	29113		315.4	32005	
318.3	31156		315.9	32375	
318.8	31546		316.4	32792	
319.3	31994	316.9	33293		
319.8	32567	317.4	32375		
320.3	34045	317.8	32792		
320.8	53497	318.3	33293		
321.3	63220	318.8	34151		
321.8	63837	319.3	38891		
322.3	64512	319.8	45843		
322.8	65297	320.3	52533		
323.3	66745	320.8	58329		
323.8	120024	321.3	63222		
324.3	120454	321.8	65257		
324.8	120828	322.3	67231		
325.3	121138	322.8	68038		
325.8	121496	323.3	69745		
326.3	121848	323.8	107967		
326.8	122184	324.3	121812		
327.3	122554	324.8	122186		
327.8	122935	325.3	122540		
328.3	123312	325.8	122912		
328.8	123692	326.3	123252		
329.3	124063	326.8	123615		
329.8	124421	330.3	126232		
330.3	124802	335.3	129973		
330.8	125175	340.3	133653		
331.3	125533	345.3	137378		
331.8	125898	350.3	141122		
335.3	128504	355.2	144942		
340.3	132407	329.2	148043		
345.3	136445				
350.2	140278				
355.2	144089				
359.2	147138				

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; γ_1 : triclinic primary solid solution; α -R-II: rhombohedral rotator phase; L : liquid phase.

$$H(T) - H(260) = \frac{3NR\theta}{\exp(\theta/T)} - H_E$$

The parameters N , θ and the integration constant H_E , are optimized by using the Rosenbrock method [18], from the temperature and enthalpy data corresponding to γ_1 , β'_1 , β'' , β'_2 and γ_2 . The results are given in Table 14.

Table 4 Variations of the enthalpy vs. temperature

T/K	$C_{24}:2.5 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:10 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0		259.5	0	
260.5	469		260.5	478	
265.5	2958		265.5	3061	
270.5	5426		270.5	5676	
275.5	7903		275.5	8424	
280.5	10631		280.5	11381	
285.4	13514		285.4	14498	
290.4	16356		290.4	17391	
295.4	19628		295.4	20563	
300.4	23310	$\gamma_1 + \beta'_1$	300.4	23888	β'_1
305.4	26952		305.4	27253	
310.4	30760		308.4	29677	
312.4	32346		308.9	30080	
312.9	32778		309.4	30503	
313.4	33283		309.9	30927	
313.9	33664		310.4	31426	
314.4	34036		310.9	31900	
314.9	38662		311.4	32377	
315.4	45479		311.9	32934	
315.8	46453	$\gamma_1 + \beta'_1$	312.4	35140	
316.3	47594	$\gamma_1 + RI$	312.9	47212	
316.8	49150		313.4	48922	
317.3	51792		313.9	49828	
317.8	54911		314.4	50684	
318.3	57796		314.9	51586	β
318.8	60713		315.4	52476	
319.3	62879		315.8	53418	
319.8	64107		316.3	54351	
320.3	64854		316.8	55249	
320.8	65469		317.3	56129	
321.3	66133	$\gamma_1 + RI$	317.8	56942	
321.8	66727		318.3	57748	RI
322.3	67382		318.8	58460	
322.8	68105	$\alpha-RII$	319.3	59116	
323.3	69199		319.8	59894	
323.8	95139		320.3	60496	
324.3	123140		320.8	61091	
324.8	123551		321.3	61754	
325.3	123978		321.8	62443	
325.8	124324		322.3	63185	$\alpha-RII$
326.3	124698		322.8	63999	
326.8	125063		323.3	64977	
330.3	127795		323.8	67693	
335.3	131741		324.3	118712	
340.3	135729	L	324.8	119521	
345.3	139784		325.3	119912	
350.2	143824		325.8	120330	
355.2	147907		326.3	120732	
359.2	151205		326.8	121127	L
			330.3	123756	
			335.3	127545	
			340.3	131512	
			345.3	135426	
			350.2	139363	
			355.2	143254	
			359.2	146479	

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; γ_1 : triclinic primary solid solution; β'_1 : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

Table 5 Variations of the enthalpy vs. temperature

T/K	$C_{24}:15.1 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:20 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0		259.5	0	
260.5	423		260.5	564	
265.5	1847		265.5	3533	
270.5	3605		270.5	6678	
275.5	5322		271.5	7305	β''
280.5	7328		272.5	7921	
285.4	9388		273.5	8445	
290.4	11760		274.5	8897	
291.4	12314	$\beta_1 + \beta''$	275.5	9047	
292.4	12858		276.5	9381	
293.4	13354		277.5	9853	
294.4	13873		278.5	10380	
295.4	14424		279.5	10834	
296.4	15051		280.5	11333	
297.4	15501		285.4	13913	
298.4	16122		290.4	16850	
299.4	16656		295.4	20010	
300.4	17262		300.4	23549	$\beta_1 + \beta''$
305.4	20454		305.4	27043	
308.4	22779	β_1	308.4	29260	
308.9	23168		308.9	29685	
309.4	23566		309.4	30082	
309.9	24015		309.9	30499	
310.4	24460		310.4	30921	
310.9	24971		310.9	31392	
311.4	25538		311.4	32092	
311.9	30422		311.9	43542	
312.4	39587		312.4	45444	
312.9	40482		312.9	46202	
313.4	41346		313.4	46954	
313.9	42184		313.9	47751	β
314.4	43081		314.4	48576	
314.9	43928		314.9	49384	
315.4	44770		315.4	50215	
315.8	45686		315.9	51081	
316.3	46585		316.4	51919	
316.8	47408		316.9	52751	
317.3	48205		317.4	53508	
317.8	48926		317.8	54175	
318.3	49602		318.3	54793	
318.8	50213	RI	318.8	55368	
319.3	50873		319.3	55957	
319.8	51512		319.8	56513	
320.3	52070		320.3	57072	
320.8	52667		320.8	57579	
321.3	53260		321.3	58143	
321.8	53810		321.8	58717	
322.3	54390		322.3	59302	α -RII
322.8	55004		322.8	59879	
323.3	55679		323.3	60479	
323.8	56331		323.8	61234	
324.3	56636		324.3	62971	
324.8	110494		324.8	83645	
325.3	110866		325.3	114690	
325.8	111259		325.8	115022	
326.3	111628		326.3	115352	
326.8	112011		326.8	115657	
330.3	114636		327.3	116003	
335.3	118406		327.8	116335	
340.3	122168		330.3	117978	
345.3	125951		335.3	121354	
350.2	129877		340.3	124690	
355.2	133717		345.3	128008	
359.2	136887		350.3	131544	
			355.2	135127	
			359.2	137920	

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; β_1' , β'' : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

Table 6 Variations of the enthalpy vs. temperature

T/K	$C_{24}:25 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:30 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0		259.5	0	
260.5	667		260.5	743	
265.5	3344		265.5	3510	
270.5	6284		270.5	6376	
275.5	9988		275.5	9485	
279.5	12373		280.5	12728	
280.5	13035		285.4	15884	
281.4	13611		290.4	19380	
282.4	14179		295.4	22965	
283.4	14841		300.4	26677	
284.4	15440		305.4	30697	
285.4	16173		308.4	33314	
290.4	19609		308.9	33887	
295.4	22970		309.4	34353	
300.4	26768		309.9	34844	
305.4	30670		310.4	35266	
308.4	33309		310.9	35873	
308.9	33676		311.4	37101	
309.4	34081		311.9	48340	
309.9	34570		312.4	51076	
310.4	34993		312.9	51830	
310.9	35571		313.4	52540	
311.4	37063		313.9	53361	
311.9	49376		314.4	54202	
312.4	50144		314.9	55080	
312.9	50935		315.4	56020	
313.4	51717		315.8	56954	
313.9	52559		316.3	57954	
314.4	53504		316.8	58763	
314.9	54339		317.3	59584	
315.4	55147		317.8	60340	
315.8	56071		318.3	60929	
316.3	56996		318.8	61544	
316.8	57794		319.3	62234	
317.3	58569		319.8	62895	
317.8	59259		320.3	63497	
318.3	59945		320.8	64211	
318.8	60581		321.3	64779	
319.3	61221		321.8	65368	
319.8	61808		322.3	65907	
320.3	62413		322.8	66373	
320.8	62993		323.3	67056	
321.3	63596		323.8	67758	
321.8	64169		324.3	68627	
322.3	64752		324.8	72487	
322.8	65319		325.3	100400	
323.3	65946		325.8	123833	
323.8	66523		326.3	124253	
324.3	67727		326.8	124658	
324.8	88404		327.3	125139	
325.3	121923		327.8	125554	
325.8	122330		330.3	127634	
326.3	122768		335.3	131686	
326.8	123232		340.3	135625	
327.3	123627		345.3	139753	
327.8	124027		350.2	143828	
330.3	126213		355.2	148013	
335.3	130241		359.2	151321	
340.3	134160				
345.3	138511				
350.2	142738				
355.2	146833				
359.2	150336				

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; β'_1 , β'' : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

Table 7 Variations of the enthalpy vs. temperature

T/K	$C_{24}:33 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:35.2 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0	β''	259.5	0	β''
260.5	363				
265.5	2730				
270.5	5463				
275.5	8495				
280.5	11660				
285.4	14826				
290.4	18244				
295.4	21500				
300.4	25173				
305.4	29068				
308.4	31743				
308.9	32204				
309.4	32569				
309.9	33026				
310.4	33530				
310.9	34143				
311.4	34761				
311.9	40674				
312.4	48870				
312.9	49669				
313.4	50533				
313.9	51377				
314.4	52179				
314.9	53040				
315.4	53871				
315.8	54757				
316.3	55737				
316.8	56466				
317.3	57225				
317.8	57915				
318.3	58572				
318.8	59143				
319.3	59783				
319.8	60375				
	60828				
320.3	61412				
320.8	61970				
321.3	62534				
321.8	63099				
322.3	63689				
322.8	64282				
323.3	64886				
323.8	65564				
324.3	66856				
324.8	88452				
325.3	121498				
325.8	121931				
326.3	122388				
326.8	122805				
327.3	123209				
327.8	123547				
330.3	129713				
335.3	134098				
340.3	138189				
345.3	142397				
350.2	146488				
355.2	149856				
359.2					
259.5		β''	259.5	0	β''
260.5	1832				
265.5	4742				
270.5	7606				
275.5	10273				
280.5	13004				
285.4	16029				
290.4	18976				
295.4	22397				
300.4	25870				
305.4	29942				
308.4	32462				
308.9	32916				
309.4	33361				
309.9	33780				
310.4	34212				
310.9	34741				
311.4	36101				
311.9	42444				
312.4	48800				
312.9	49688				
313.4	50446				
313.9	51328				
314.4	52136				
314.9	52984				
315.4	53928				
315.8	54891				
316.3	55773				
316.8	56586				
317.3	57412				
317.8	58134				
318.3	58721				
318.8	59324				
319.3	59938				
319.8	60611				
320.3	61248				
320.8	61837				
321.3	62437				
321.8	63035				
322.3	63518				
322.8	64276				
323.3	65038				
323.8	65895				
324.3	67155				
324.8	70647				
325.3	86481				
325.8	121252				
326.3	121676				
326.8	122043				
327.3	122444				
327.8	122839				
330.3	124831				
335.3	128967				
340.3	133060				
345.3	137300				
350.2	141457				
355.2	145562				
359.2	148834				

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; β'' : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

As an example, results obtained for pure n - $C_{24}H_{50}$ are presented in Fig. 4, which shows the variation in the error function F with θ .

Table 8 Variations of the enthalpy vs. temperature

T/K	$C_{24}:40.1 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:45.1 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0		259.5	0	
260.5	390		260.5	460	
265.5	2731		265.5	3220	
270.5	5645		270.5	5926	
275.5	8789		271.5	6477	
280.5	12053		272.5	6880	
285.4	15128		273.5	7259	
290.4	18490		274.5	7773	
295.4	21569		275.5	8394	
300.4	25298		276.5	8948	
305.4	29257		277.5	9631	
309.4	32565		278.5	10221	
309.9	33059		279.5	10888	
310.4	33563		280.5	11335	
310.9	34017		285.4	14386	
311.4	34536		300.4	17633	
311.9	36313		295.4	21007	
312.4	43461		300.4	24499	
312.9	48702		305.4	28321	
313.4	49773		309.4	31723	
313.9	50735		309.9	32177	
314.4	51511		310.4	32619	
314.9	52329		310.9	33055	
315.4	53206		311.4	33652	
315.8	54091		311.9	34911	
316.3	54971		312.4	38960	
316.8	55845		312.9	44666	
317.3	56661		313.4	48124	
317.8	57378		313.9	49067	
318.3	58086		314.4	49920	
318.8	58645		314.9	50771	
319.3	59253		315.4	51690	
319.8	59876		315.8	52614	
320.3	60438		316.3	53565	
320.8	61040		316.8	54425	
321.3	61605		317.3	55299	
321.8	62138		317.8	56074	
322.3	62719		318.3	56705	
322.8	63327		318.8	57327	
323.3	63924		319.3	57971	
323.8	64515		319.8	58596	
324.3	65175		320.3	59189	
324.8	65927		320.8	59826	
325.3	66807		321.3	60474	
325.8	67454		321.8	61083	
326.3	68168		322.3	61668	
326.8	68847		322.8	62327	
327.3	69493		323.3	62851	
327.8	70188		323.8	63459	
328.3	70929		324.3	64030	
328.8	71692		324.8	64636	
329.3	72498		325.3	65760	
329.8	73456		325.8	66861	
330.3	74489		326.3	68076	
330.8	75582		326.8	69395	
331.3	76738		327.3	70819	
331.8	77959		327.8	72339	
332.3	79247		328.3	73964	
332.8	80603		328.8	75694	
333.3	82028		329.3	77539	
333.8	83523		329.8	79499	
334.3	85089		330.3	81574	
334.8	86727		330.8	83764	
335.3	88438		331.3	86079	
335.8	90223		331.8	88519	
336.3	92084		332.3	91094	
336.8	94021		332.8	93804	
337.3	96036		333.3	96649	
337.8	98129		333.8	99629	
338.3	100302		334.3	102744	
338.8	102557		334.8	105994	
339.3	104894		335.3	109379	
339.8	107315		335.8	112909	
340.3	109821		336.3	116484	
340.8	112414		336.8	120214	
341.3	115095		337.3	124099	
341.8	117866		337.8	128139	
342.3	120727		338.3	132334	
342.8	123679		338.8	136684	
343.3	126723		339.3	141189	
343.8	129860		339.8	145849	
344.3	133091		340.3	150664	
344.8	136417		340.8	155634	
345.3	139840		341.3	160759	
345.8	143361		341.8	166039	
346.3	146980		342.3	171474	
346.8	150699		342.8	177074	
347.3	154518		343.3	182839	
347.8	158439		343.8	188769	
348.3	162462		344.3	194864	
348.8	166587		344.8	201124	
349.3	170814		345.3	207549	
349.8	175143		345.8	214139	
350.3	179574		346.3	220894	
350.8	184107		346.8	227814	
351.3	188743		347.3	234899	
351.8	193482		347.8	242149	
352.3	198324		348.3	249564	
352.8	203269		348.8	257144	
353.3	208317		349.3	264889	
353.8	213469		349.8	272799	
354.3	218725		350.3	280874	
354.8	224086		350.8	289014	
355.3	229553		351.3	297319	
355.8	235126		351.8	305789	
356.3	240805		352.3	314424	
356.8	246590		352.8	323224	
357.3	252481		353.3	332189	
357.8	258478		353.8	341319	
358.3	264582		354.3	350614	
358.8	270793		354.8	360074	
359.3	277111		355.3	369699	
359.8	283536		355.8	379489	
360.3	290069		356.3	389444	
360.8	296711		356.8	399564	
361.3	303462		357.3	409849	
361.8	310323		357.8	420299	
362.3	317294		358.3	430914	
362.8	324375		358.8	441694	
363.3	331566		359.3	452639	
363.8	338867		359.8	463749	
364.3	346278		360.3	475024	
364.8	353799		360.8	486464	
365.3	361430		361.3	498069	
365.8	369171		361.8	509839	
366.3	377022		362.3	521774	
366.8	384983		362.8	533874	
367.3	393054		363.3	546139	
367.8	401235		363.8	558569	
368.3	409526		364.3	571164	
368.8	417927		364.8	583924	
369.3	426438		365.3	596849	
369.8	435059		365.8	609939	
370.3	443790		366.3	623194	
370.8	452631		366.8	636614	
371.3	461582		367.3	650199	
371.8	470643		367.8	663949	
372.3	479814		368.3	677864	
372.8	489095		368.8	691944	
373.3	498486		369.3	706189	
373.8	507987		369.8	720599	
374.3	517598		370.3	735174	
374.8	527319		370.8	749914	
375.3	537150		371.3	764819	
375.8	547091		371.8	779889	
376.3	557142		372.3	795124	
376.8	567303		372.8	810524	
377.3	577574		373.3	826089	
377.8	587955		373.8	841819	
378.3	598446		374.3	857714	
378.8	609047		374.8	873774	
379.3	619758		375.3	889999	
379.8	630579		375.8	906389	
380.3	641510		376.3	922944	
380.8	652551		376.8	939664	
381.3	663702		377.3	956549	
381.8	674963		377.8	973699	
382.3	686334		378.3	991014	
382.8	697815		378.8	1008494	
383.3	709406		379.3	1027139	
383.8	721107		379.8	1045949	
384.3	732918		380.3	1064924	
384.8	744839		380.8	1084064	
385.3	756870		381.3	1103369	
385.8	769021		381.8	1122839	
386.3	781282		382.3	1142474	
386.8	793653		382.8	1162274	
387.3	806134		383.3	1182239	
387.8	818725		383.8	1202369	
388.3	831426		384.3	1222564	
388.8	844237		384.8	1242924	
389.3	857158		385.3	1263449	
389.8	870189		385.8	1284139	
390.3	883330		386.3	1304994	
390.8	896581		386.8	1326014	
391.3	909942		387.3	1347199	
391.8	923413		387.8	1368549	
392.3	936994		388.3	1390064	
392.8	950685		388.8	1411744	
393.3	964486		389.3	1433589	
393.8	978397		389.8	1455599	
394.3	992418		390.3	1477774	
394.8	1006549		390.8	1499914	
395.3	1020790		391.3	1522119	
395.8	1035141		391.8	1544489	
396.3	1049602		392.3	1566924	
396.8	1064173		392.8	1589524	
397.3	1078854		393.3	1612289	
397.8	1093645		393.8	1635219	
398.3	1108546		394.3	1658314	
398.8	1123557		394.8	1681574	
399.3	1138678		395.3	1704999	
399.8	1153909		395.8	1728589	
400.3	1169250		396.3	1752344	
400.8	1184701		396.8	1776264	
401.3	1200262		397.3	1800349	
401.8	1215933		397.8	1824589	
402.3	1231714		398.3	1848994	
402.8	1247605		398.8	1873564	
403.3	1263606		399.3	1898299	
403.8	1279717		399.8	1923199	
404.3	1295938		400.3	1948264	
404.8	1312269		400.8	1973494	
405.3	1328710		401.3	1998889	
405.8	1345261		401.8	2024449	
406.3	1361922		402.3	2050174	
406.8	1378693		402.8	2076064	
407.3	1395574		403.3	2102119	
407.8	1412565		403.8	2128339	
408.3	1429666		404.3	2154714	
408.8	1446877		404.8	2181254	
409.3	1464198		405.3	2207959	
409.8	1481629		405.8	2234829	
410.3	1499170		406.3	2261864	
410.8	1516821		406.8	2289064	
411.3	1534582		407.3	2316429	
411.8	1552453		407.8	2343959	
412.3	1570434		408.3	2371654	
412.8	1588525		408.8	2399514	
413.3	1606726		409.3	2427539	
413.8					

Table 9 Variations of the enthalpy vs. temperature

T/K	$C_{24}:49.8 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:60.1 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase		
259.5	0	↕ $\beta'' + \beta'_2$	259.5	0	↕ $\beta'' + \beta'_2$		
260.5	612						
265.5	3156						
270.5	5644						
275.5	8463						
280.5	10976						
285.4	14033						
290.4	16829						
295.4	18665						
300.4	21940						
305.4	25426	↕ β	297.4	22922	↕ β'_2		
309.4	28317						
309.4	28746						
310.4	29149						
310.9	29567						
311.4	30032						
311.9	30537						
312.4	31414						
312.9	33830						
313.4	38334						
313.9	43284	↕ β	298.4	23639	↕ $\beta'' + \beta'_2$		
314.4	46457						
314.9	47307						
315.4	48131						
315.8	48974						
316.3	49818						
316.8	50686						
317.3	51541						
317.8	52326						
318.3	53017						
318.8	53674	↕ β	299.4	24396	↕ $\beta'' + \beta'_2$		
319.3	54258						
319.8	54847						
320.3	55443						
320.8	56005						
321.3	56583						
321.8	57122						
322.3	57662						
322.8	58216						
323.3	58766						
323.8	59346	↕ β	300.4	25212	↕ $\beta'' + \beta'_2$		
324.3	59926						
324.8	60579						
325.3	61368						
325.8	63096						
326.3	79507						
326.8	115901						
327.3	117423						
327.8	117842						
330.3	119712						
335.3	123514	↕ β	305.4	29100	↕ $\beta'' + \beta'_2$		
340.3	127349						
345.3	131216						
350.2	135081						
355.2	139004						
359.2	142072						
			↕ β	310.4		33276	↕ $\beta'' + \beta'_2$
		↕ β	310.9	33802	↕ $\beta'' + \beta'_2$		
		↕ β	311.4	34258	↕ $\beta'' + \beta'_2$		
		↕ β	311.9	34754	↕ $\beta'' + \beta'_2$		
		↕ β	312.4	35303	↕ $\beta'' + \beta'_2$		
		↕ β	312.9	36190	↕ $\beta'' + \beta'_2$		
		↕ β	313.4	37608	↕ $\beta'' + \beta'_2$		
		↕ β	313.9	40388	↕ $\beta'' + \beta'_2$		
		↕ β	314.4	44697	↕ $\beta'' + \beta'_2$		
		↕ β	314.9	48704	↕ $\beta'' + \beta'_2$		
		↕ β	315.4	51868	↕ $\beta'' + \beta'_2$		
		↕ β	315.9	53228	↕ $\beta'' + \beta'_2$		
		↕ β	316.4	54232	↕ $\beta'' + \beta'_2$		
		↕ β	316.9	55153	↕ $\beta'' + \beta'_2$		
		↕ β	317.4	56043	↕ $\beta'' + \beta'_2$		
		↕ β	317.8	56985	↕ $\beta'' + \beta'_2$		
		↕ β	318.3	57794	↕ $\beta'' + \beta'_2$		
		↕ β	318.8	58595	↕ $\beta'' + \beta'_2$		
		↕ β	319.3	59264	↕ $\beta'' + \beta'_2$		
		↕ β	319.8	59923	↕ $\beta'' + \beta'_2$		
		↕ β	320.3	60475	↕ $\beta'' + \beta'_2$		
		↕ β	320.8	61052	↕ $\beta'' + \beta'_2$		
		↕ β	321.3	61687	↕ $\beta'' + \beta'_2$		
		↕ β	321.8	62333	↕ $\beta'' + \beta'_2$		
		↕ β	322.3	62903	↕ $\beta'' + \beta'_2$		
		↕ β	322.8	63478	↕ $\beta'' + \beta'_2$		
		↕ β	323.3	64128	↕ $\beta'' + \beta'_2$		
		↕ β	323.8	64770	↕ $\beta'' + \beta'_2$		
		↕ β	324.3	65373	↕ $\beta'' + \beta'_2$		
		↕ β	324.8	66000	↕ $\beta'' + \beta'_2$		
		↕ β	325.3	66716	↕ $\beta'' + \beta'_2$		
		↕ β	325.8	67545	↕ $\beta'' + \beta'_2$		
		↕ β	326.3	70352	↕ $\beta'' + \beta'_2$		
		↕ β	326.8	93601	↕ $\beta'' + \beta'_2$		
		↕ β	327.3	124562	↕ $\beta'' + \beta'_2$		
		↕ β	327.8	124996	↕ $\beta'' + \beta'_2$		
		↕ β	328.3	125412	↕ $\beta'' + \beta'_2$		
		↕ β	328.8	125778	↕ $\beta'' + \beta'_2$		
		↕ β	329.3	126142	↕ $\beta'' + \beta'_2$		
		↕ β	329.8	126535	↕ $\beta'' + \beta'_2$		
		↕ β	330.3	126998	↕ $\beta'' + \beta'_2$		
		↕ β	335.3	131109	↕ $\beta'' + \beta'_2$		
		↕ β	340.3	135350	↕ $\beta'' + \beta'_2$		
		↕ β	345.3	139522	↕ $\beta'' + \beta'_2$		
		↕ β	350.3	143752	↕ $\beta'' + \beta'_2$		
		↕ β	355.2	148014	↕ $\beta'' + \beta'_2$		
		↕ β	359.2	151528	↕ $\beta'' + \beta'_2$		

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; β'' , β'_2 : orthorhombic intermediate solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

Table 10 Variations of the enthalpy vs. temperature

<i>T</i> /K	<i>C</i> ₂₄ :75 mol% <i>C</i> ₂₆ <i>H</i> ²⁶⁰ (<i>T</i>)/J mol ⁻¹	Phase	<i>T</i> /K	<i>C</i> ₂₄ :77.1 mol% <i>C</i> ₂₆ <i>H</i> ²⁶⁰ (<i>T</i>)/J mol ⁻¹	Phase
259.5	0	β ₂	259.5	0	β ₂
260.5	682				
265.5	3513				
270.5	6550				
275.5	9282				
280.5	12393				
285.4	15812				
290.4	18986				
295.4	22268				
300.4	25965				
305.4	29822				
310.4	34027				
313.4	36703				
313.9	37236				
314.4	37930				
314.9	38758				
315.4	39894				
315.8	41569				
316.3	43905				
316.8	47487				
317.3	51901				
317.8	55754				
318.3	58379				
318.8	59678				
319.3	60836				
319.8	61434				
320.3	62218				
320.8	62898				
321.3	63576				
321.8	64232				
322.3	64881				
322.8	65497				
323.3	66147				
323.8	66731				
324.3	67383				
324.8	68039				
325.3	68782				
325.8	69470				
326.3	70218				
326.8	71254				
327.3	75834				
327.8	98933				
328.3	128734				
328.8	129166				
329.3	129588				
329.8	129995				
330.3	130425				
335.3	134434				
340.3	138514				
345.3	142622				
350.2	146579				
355.2	150827				
359.2	154193				
322.8	65695	β	316.3	42687	β
323.3	66147				
323.8	66731				
324.3	67383				
324.8	68039				
325.3	68782				
325.8	69470				
326.3	70218				
326.8	71254				
327.3	75834				
327.8	98970				
328.3	126301				
328.8	126746				
329.3	127209				
329.8	127653				
330.3	128072				
335.3	132365				
340.3	136761				
345.3	141157				
350.2	145503				
355.2	149931				
359.2	153440				
321.8	63206	α-RII	317.3	48963	α-RII
322.3	63841				
322.8	64454				
323.3	65068				
323.8	65695				
324.3	66313				
324.8	66924				
325.3	67554				
325.8	68205				
326.3	68934				
326.8	69792				
327.3	71990				
327.8	89670				
328.3	126301				
328.8	126746				
329.3	127209				
329.8	127653				
330.3	128072				
335.3	132365				
340.3	136761				
345.3	141157				
350.2	145503				
355.2	149931				
359.2	153440				
320.3	61233	L	319.8	60427	L
320.8	61931				
321.3	62583				
321.8	63206				
322.3	63841				
322.8	64454				
323.3	65068				
323.8	65695				
324.3	66313				
324.8	66924				
325.3	67554				
325.8	68205				
326.3	68934				
326.8	69792				
327.3	71990				
327.8	89670				
328.3	126301				
328.8	126746				
329.3	127209				
329.8	127653				
330.3	128072				
335.3	132365				
340.3	136761				
345.3	141157				
350.2	145503				
355.2	149931				
359.2	153440				

T: temperature in Kelvins; *H*²⁶⁰(*T*): measured enthalpy, with *T*=260 K as reference, in Joule per mol; β₂: orthorhombic intermediate solid solution; β-RI: orthorhombic rotator phase; α-RII: rhombohedral rotator phase; *L*: liquid phase.

The general function *F* is defined by

$$F(\theta, x) = \sum_{i=1}^n ((\Delta H(x)_{\text{exp}} - \Delta H(\theta, x)_{\text{calc}})^2)$$

where $\Delta H(x)_{\text{exp}}$ is the variation in enthalpy measured for each molar fraction x ; $\Delta H(\theta, x)_{\text{calc}}$ is the variation in enthalpy calculated for each molar fraction x ; and n is the number of points taken into account for the optimization.

Deviations between calculated and experimental data are illustrated in Fig. 5. The agreement between the experimental and calculated values is very good (less than 2 J mol^{-1}).

Table 11 Variations of the enthalpy vs. temperature

T/K	$C_{24}:80 \text{ mol}\% C_{26}$ $H^{260}(T)/\text{J mol}^{-1}$	Phase	T/K	$C_{24}:90.1 \text{ mol}\% C_{26}$ $H^{260}(T)/\text{J mol}^{-1}$	Phase
259.5	0	β_2	259.5	0	$\beta_2 + \gamma_2$
260.5	424		260.5	380	
265.5	3042		265.5	2065	
270.5	5795		270.5	4810	
275.5	8622		275.5	7441	
280.5	11496		280.5	10160	
285.4	14491		285.4	13084	
290.4	17434		290.4	16043	
295.4	20958		295.4	19211	
300.4	24270		300.4	22451	
305.4	27618		305.4	25981	
310.4	31283		310.4	29573	
314.4	34332		315.4	33335	
314.9	34857		318.3	35934	
315.4	35455		318.8	36533	
315.8	36223	319.3	37467		
316.3	37395	319.8	39279		
316.8	39262	320.3	43029		
317.3	42037	320.8	50663		
317.8	45326	321.3	58666		
318.3	50014	321.8	61051		
318.8	54487	322.3	62437		
319.3	57302	322.8	63692		
319.8	58464	323.3	64432		
320.3	59249	323.8	65043		
320.8	59925	324.3	65622		
321.3	60591	324.8	66247		
321.8	61152	325.3	66834		
322.3	61759	325.8	67426		
322.8	62403	326.3	67985		
323.3	62945	326.8	68572		
323.8	63566	327.3	69154		
324.3	64115	327.8	69805		
324.8	64744	328.3	70607		
325.3	65386	328.8	73632		
325.8	66005	329.3	724016		
326.3	66682	329.8	124108		
326.8	67450	330.3	124482		
327.3	69302	335.3	128884		
327.8	79710	340.3	133112		
328.3	121862	345.3	137075		
328.8	125229	350.2	141253		
329.3	125660	355.2	145221		
329.8	126133	359.2	148493		
330.3	126515				
335.3	130537				
340.3	134586				
345.3	138749				
350.2	143033				
355.2	147281				
359.2	150826				

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260 \text{ K}$ as reference, in Joule per mol; β_2 : orthorhombic intermediate solid solution; γ_2 : triclinic primary solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

Table 12 Variations of the enthalpy vs. temperature

T/K	$C_{24}:97 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase	T/K	$C_{24}:99 \text{ mol\% } C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0	↑ γ ₂ ↓	259.5	0	↑ γ ₂ ↓
260.5	585				
265.5	3363				
270.5	6352				
275.5	8958				
280.5	11744				
285.4	14526				
290.4	17631				
295.4	20567				
300.4	23806				
305.4	27235				
310.4	30722				
315.4	34289				
320.3	37980				
320.8	38478				
321.3	38965				
321.8	39529				
322.3	40321				
322.8	41592				
323.3	44263				
323.8	50029				
324.3	58861				
324.8	70237				
325.3	73408				
325.8	74043				
326.3	74699				
326.8	75369				
327.3	76085				
327.8	76803				
328.3	77667				
328.8	80875				
329.3	113602				
329.8	136918				
330.3	137385				
330.8	137835				
331.3	138279				
331.8	138723				
335.3	141741				
340.3	146183				
345.3	150666				
350.3	155263				
355.2	159764				
359.2	163315				
329.8	137278				
330.3	137708				
330.8	138108				
331.3	138535				
331.8	138971				
335.3	141902				
340.3	146060				
345.3	150291				
350.2	154517				
355.2	158768				
359.2	162270				
328.8	80818				
328.3	78293				
327.8	77231				
327.3	76433				
326.8	75721				
326.3	75039				
325.8	74380				
325.3	66645				
324.8	51747				

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; γ_2 : triclinic primary solid solution; β -RI: orthorhombic rotator phase; α -RII: rhombohedral rotator phase; L : liquid phase.

A general expression for the enthalpy $H(T,x)$ as a function of temperature and composition can be established by study of the variation in the parameters N and θ with composition.

A dispersion of θ around 1300 K (Fig. 6) is observed and a mean value of 1367 K is chosen.

The parameter N is then calculated for each composition, with its Einstein temperature. Figure 7 presents the variation in N with composition.

The distribution of the points leads to a parabolic representation of N vs. composition:

$$N(x) = 107(1 - x) + 118.5x + 98x(1 - x)$$

where x is the molar fraction in n - $C_{26}H_{54}$ of the pure phases.

Table 13 Variations of the enthalpy vs. temperature

T/K	$C_{24}:97 \text{ mol}\% C_{26}$ $H^{260}(T)/J \text{ mol}^{-1}$	Phase
259.5	0	↑ γ ₂ ↓
260.5	274	
265.5	3432	
270.5	6310	
275.5	9195	
280.5	12349	
285.4	15383	
290.4	18679	
295.4	21968	
300.4	25213	
305.4	25562	
310.4	31935	
315.4	35366	
320.3	38989	
323.3	41337	
323.8	41767	
324.3	42241	
<hr/>		
324.8	42828	↑ α-RII↓
325.3	44529	
325.8	66706	
326.3	76661	
326.8	77304	
327.3	77961	
327.8	78623	
328.3	79323	
328.8	80076	
<hr/>		
329.3	89017	↑ L↓
329.8	140083	
330.3	140498	
330.8	140930	
331.3	141359	
335.3	144717	
340.3	148983	
345.3	153276	
350.2	157651	
355.2	162074	
359.2	165632	

T : temperature in Kelvins; $H^{260}(T)$: measured enthalpy, with $T=260$ K as reference, in Joule per mol; γ_2 : triclinic primary solid solution; α -RII: rhombohedral rotator phase; L : liquid phase.

This expression is computed in the whole range of concentration as the phase domains are too narrow for individual numerical optimization.

Nevertheless, $N(x)$ is only valid in the pure phase domains.

Finally, a general expression for the enthalpy $H(T,x)$ as a function of temperature and composition is defined for the phases γ_1 , β'_1 , β'' , β'_2 and γ_2 :

$$H(T,x) = \frac{3R\theta N(x)}{\exp(\theta/T) - 1}$$

The agreement between the experimental and calculated values is good; the mean deviation is 5%.

Conclusion

In this work, we have determined the variation in the enthalpies of n - $C_{24}H_{50}$, n - $C_{26}H_{54}$ and 19 binary mixtures between 260 and 360 K. These data for binary

Table 14 Parameters N , θ and H_E vs. composition in $n\text{-C}_{26}\text{H}_{54}$

$x/\text{mol } \% \text{ in } n\text{-C}_{26}\text{H}_{54}$	Phase	Temperature domain/ K	N	$\theta/$ K	$H_E/$ J mol^{-1}	Error function 10^{-5} F/ J mol^{-1}
0	γ_1	269.5–317.8	61.3	1093.8	24695	1.417792
1.1	γ_1	292.4–314.9	311.3	1869.4	7341	0.7135303
10	β'_1	270.5–309.4	82.8	1157	27915	4.878368
30.1	β''	270.5–309.4	113.5	1263.7	27327	1.025291
33	β''	270.5–307.4	99.9	1214.3	28844	5.314301
35.2	β''	270.5–307.4	245.7	1667.6	13823	4.443181
40.1	β''	270.5–306.4	122.0	1318.3	24966	10.12776
45.1	β''	270.5–309.9	158.8	1462.3	20331	4.890922
75	β'_2	294.4–321.4	352.6	1820	11556	4.589846
77.1	β'_2	295.4–313.4	118.1	1297.3	25299	4.927112
80	β'_2	270.5–313.4	86.6	1177.1	27325	2.765067
97	γ_2	294.4–318.3	69.7	1064.9	31227	0.4958911
99	γ_2	282.4–318.3	65.4	1020.5	33797	1.9759240
100	γ_2	270.5–321.8	45.3	774.3	46693	1.748367

mixtures of the different phases γ_1 , β'_1 , β'' , β'_2 and γ_2 , and also the phases of the pure *n*-alkanes, have been represented by an analytical expression, derived from Einstein's model of the solid state.

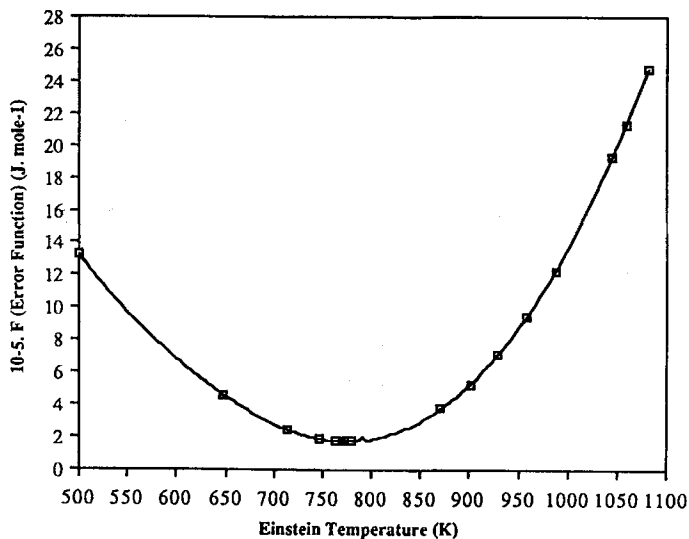


Fig. 4 Variation of the error function vs. the Einstein temperature of the *n*-hexacosane

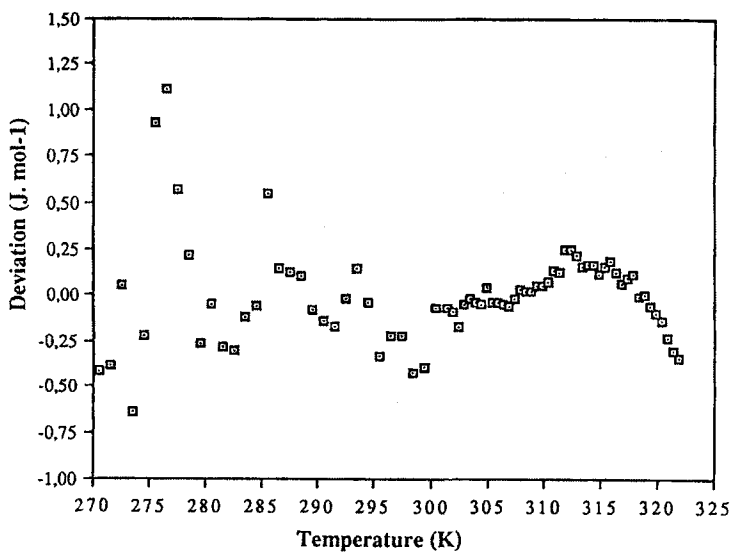


Fig. 5 Deviation between measured and calculated enthalpies

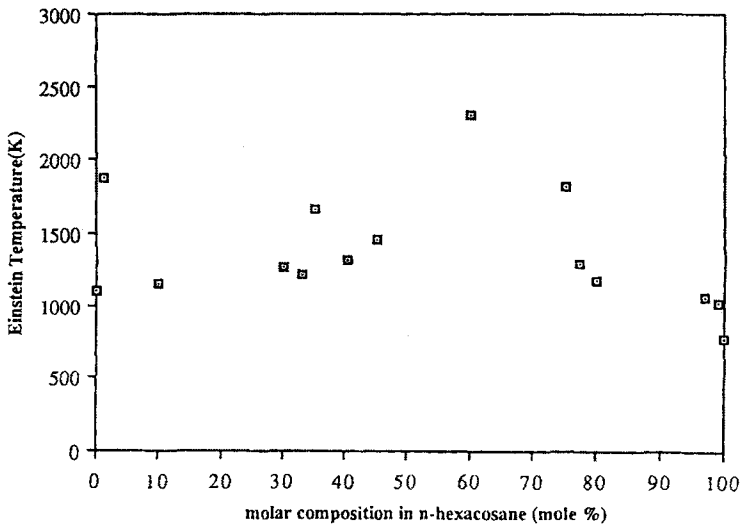


Fig. 6 Einstein temperature vs. composition

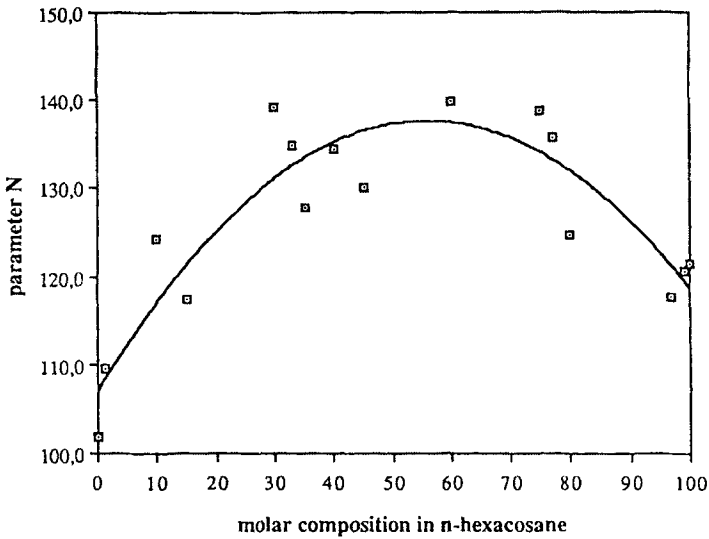


Fig. 7 Values of the parameter N vs. composition, with a constant Einstein temperature of 1367 K

A general expression has been defined for the enthalpy as a function of temperature and the molar fraction of $n\text{-C}_{26}\text{H}_{54}$.

This study gives new results on the binary system $n\text{-C}_{24}\text{H}_{50}$ – $n\text{-C}_{26}\text{H}_{54}$. These results could be used for determination of the thermodynamic functions of mixing, necessary for calculations on the solid-solid equilibria.

References

- 1 Z. Achour, J. B. Bourdet, M. Bouroukba and M. Dirand, *J. Chim. Phys.*, 90 (1993) 325.
- 2 Z. Achour-Boudjema, J. B. Bourdet, D. Petitjean and M. Dirand, *J. Mol. Struct.*, 354 (1995) 197.
- 3 H. Lüth and S. G. Nyburg, *Mol. Cryst. Liq. Cryst.*, 27 (1974) 337.
- 4 N. Hasnaoui, J. Dellacherie, L. Schuffenecker, M. Dirand and D. Balesdent, *J. Chim. Phys.*, 85 (1988) 153.
- 5 Z. Achour, J. B. Bourdet, M. Bouroukba and M. Dirand, *J. Chim. Phys.*, 89 (1992) 707.
- 6 J. Doucet, I. Denicolo, A. Craievich and A. Collet, *J. Chem. Phys.*, 75 (1981) 5125.
- 7 R. G. Snyder, A. F. Maroncelli, S. P. Qi and H. L. Strauss, *Science*, 214 (1981) 188.
- 8 I. Denicolo, A. F. Craievich and J. Doucet, *J. Chem. Phys.*, 80 (1984) 6200.
- 9 G. Ungar, *J. Phys. Chem.*, 87 (1983) 689.
- 10 S. K. Filatov, E. N. Kotelnikova and E. A. Aleksandrova, *Zeitschrift für Kristallographie*, 172 (1985) 35.
- 11 G. Ungar and N. Masic, *J. Phys. Chem.*, 89 (1985) 1036.
- 12 N. Hasnaoui, J. Dellacherie, L. Schuffenecker and M. Dirand, *J. Chim. Phys.*, 85 (1988) 675.
- 13 I. Denicolo, J. Doucet and A. F. Craievich, *J. Chem. Phys.*, 78 (1983) 1465.
- 14 J. Doucet and A. J. Dianoux, *J. Chem. Phys.*, 81 (1984) 5043.
- 15 Z. Achour, J. B. Bourdet, M. Bouroukba and M. Dirand, *J. Chim. Phys.*, 89 (1992) 707.
- 16 D. A. Ditmars, S. Ishihara, S. S. Chang and G. Bernstein, *J. Research*, 87 (1982) 159.
- 17 R. J. L. Andon and J. F. Martin, *J. Chem. Thermodynamics*, 8 (1976) 1159.
- 18 H. H. Rosenbrock, *J. 3.*, 175 (1960).